

Chapter 3

Kinetics of Electrode Reactions

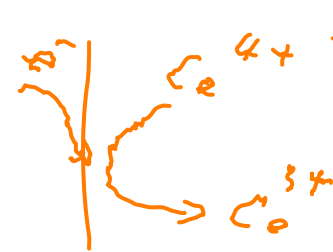
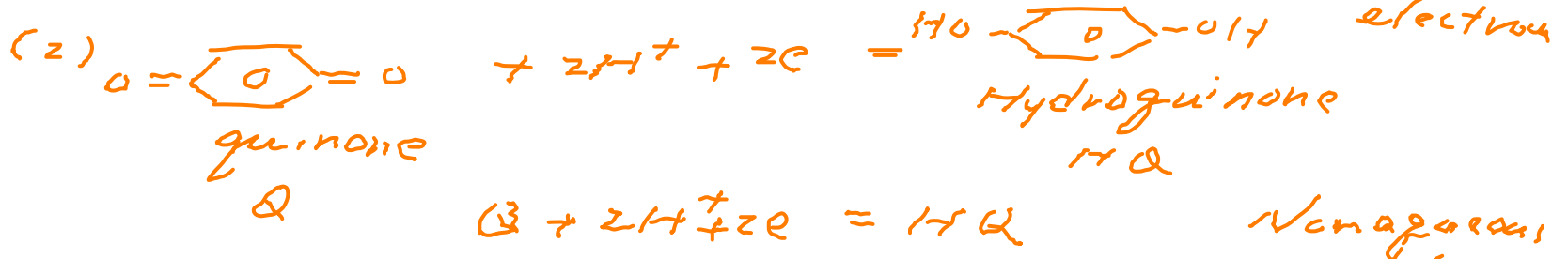
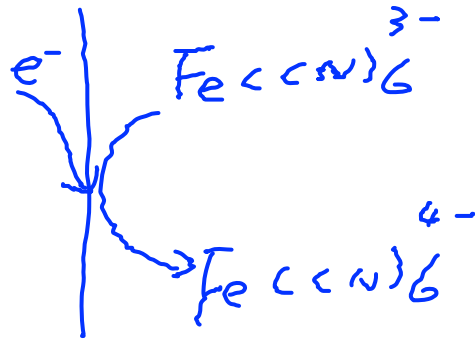
Bing Joe Hwang

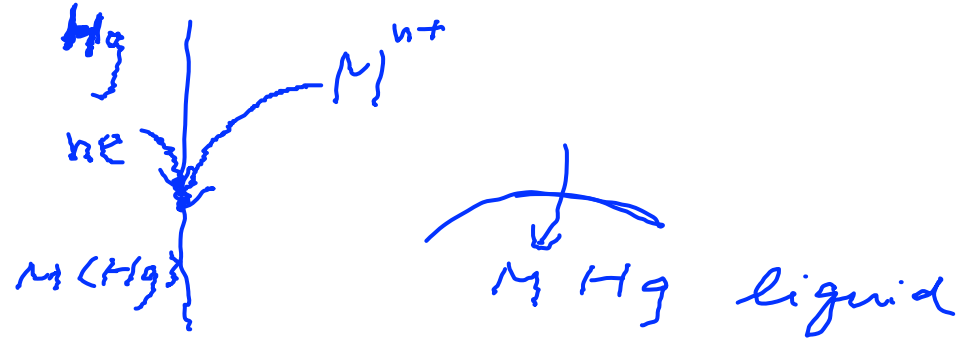
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- 1. Simple electrode reactions-**
 - 1) products dissolved in the ionic conductor**
 - 2) Products dissolved in the electron conductor**
- 2. Formation a new phase**
 - 1) Solid phase**
 - 2) Gas phase**
- 3. Electronic conductor is destroyed**
- 4. Film transformation**

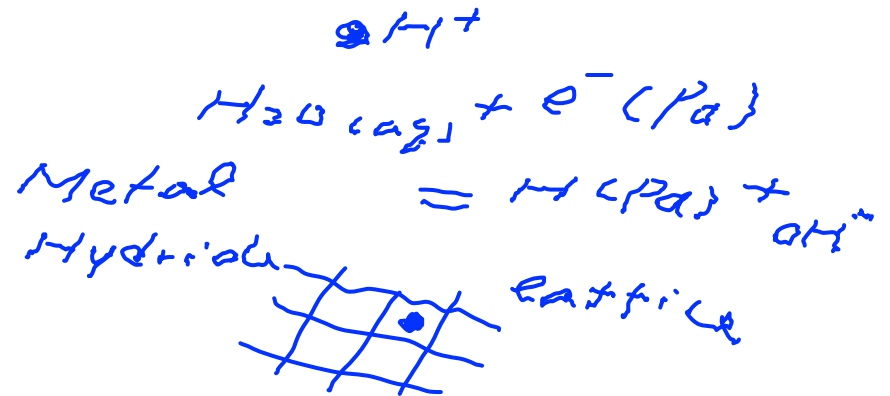
Simple Electrode rxns

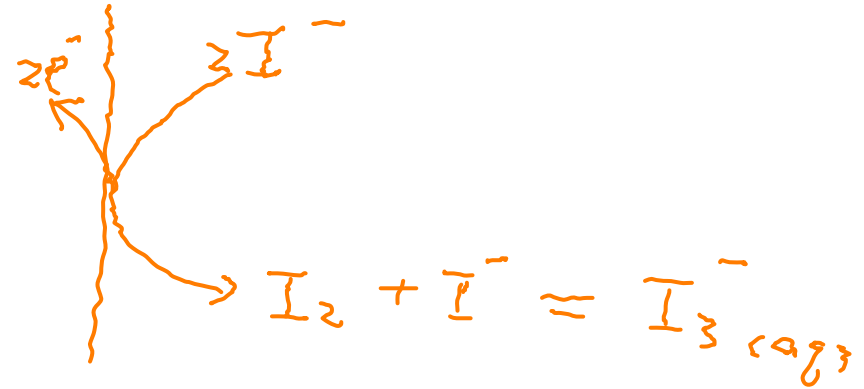
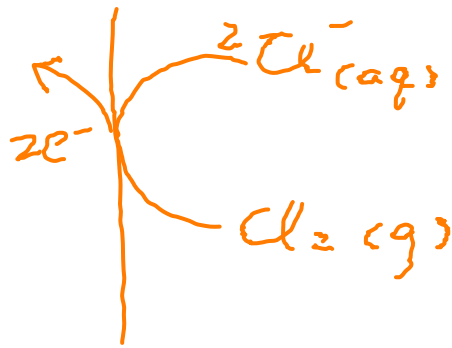




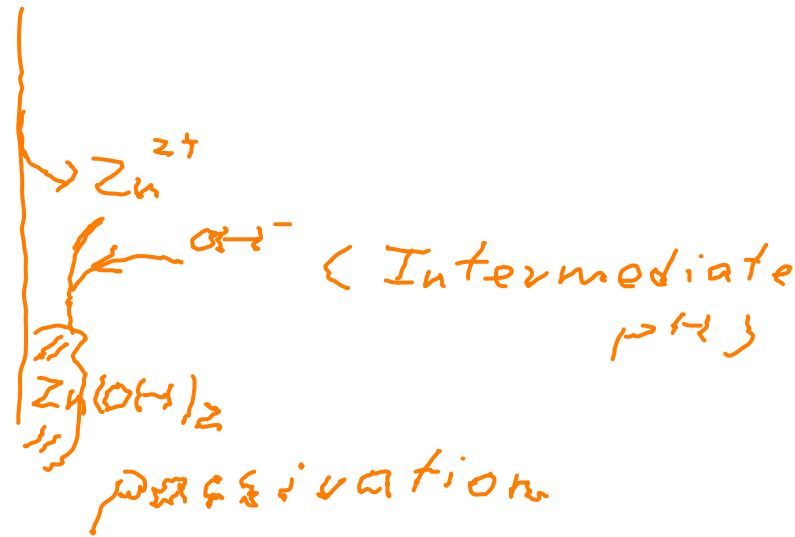
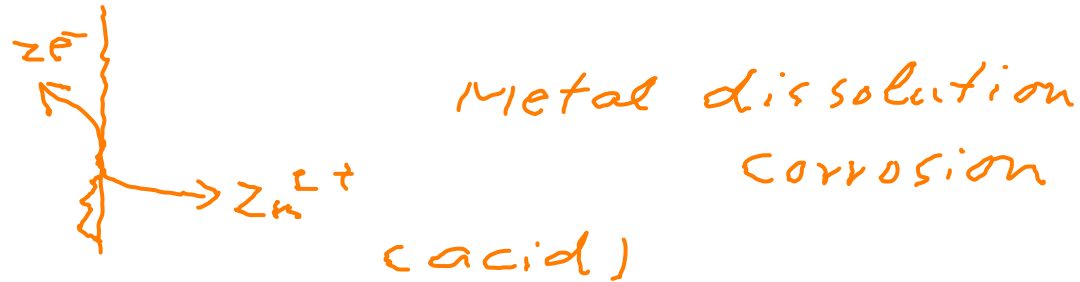
Formation of New phase

(5)

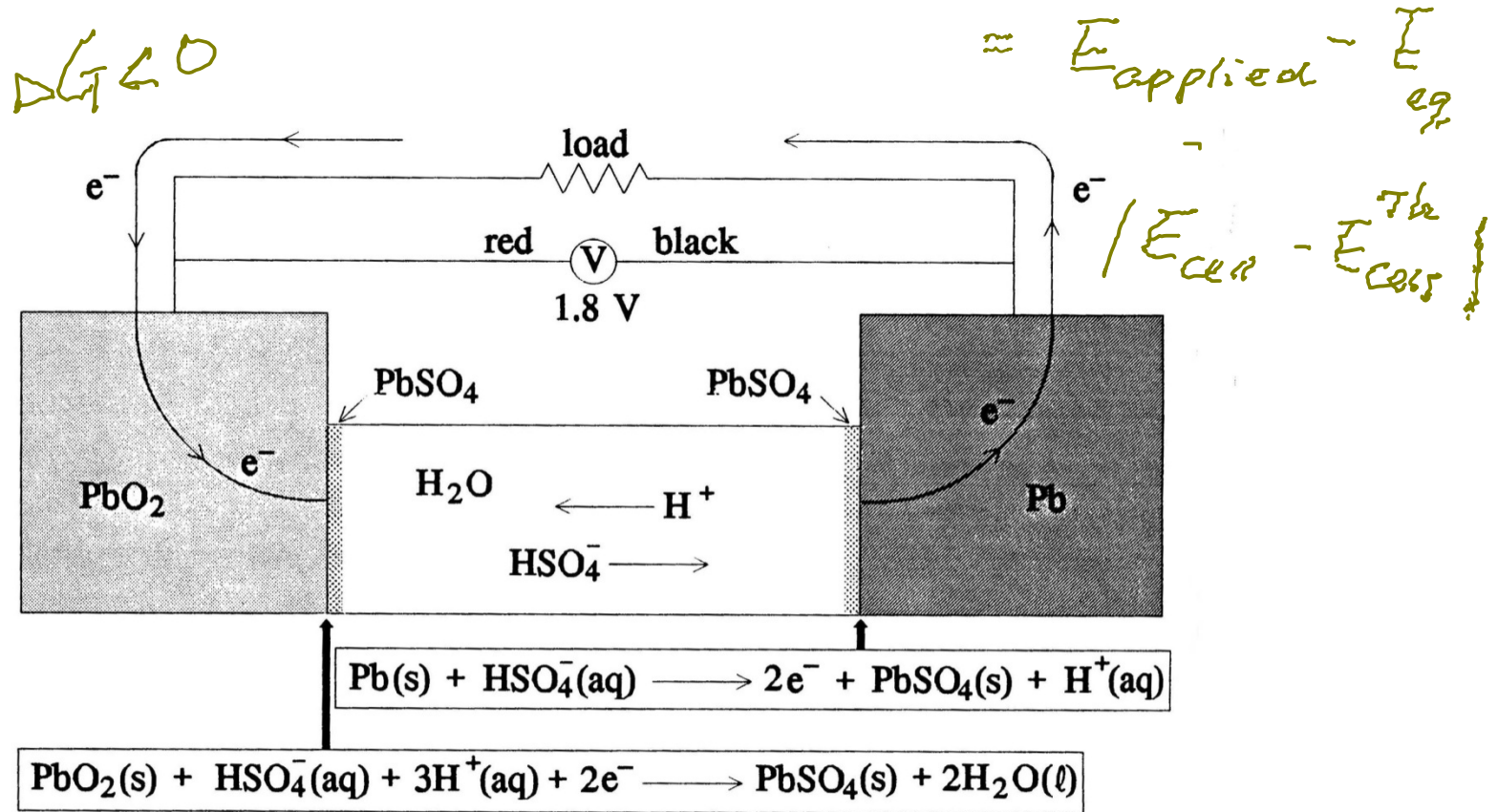




Electrode is destroyed



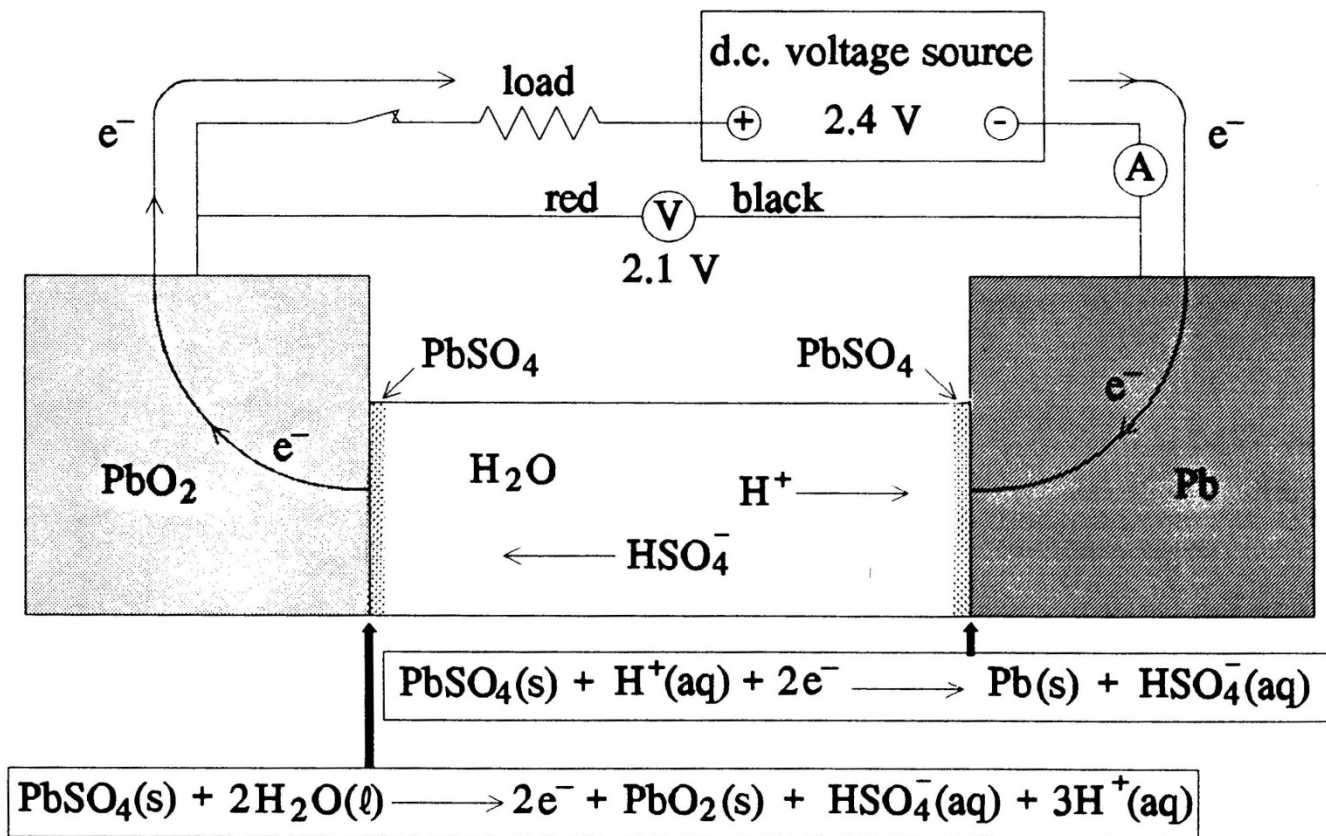
Polarization-Discharging



Polarization: their voltages decrease in magnitude when the energy is taken from them.

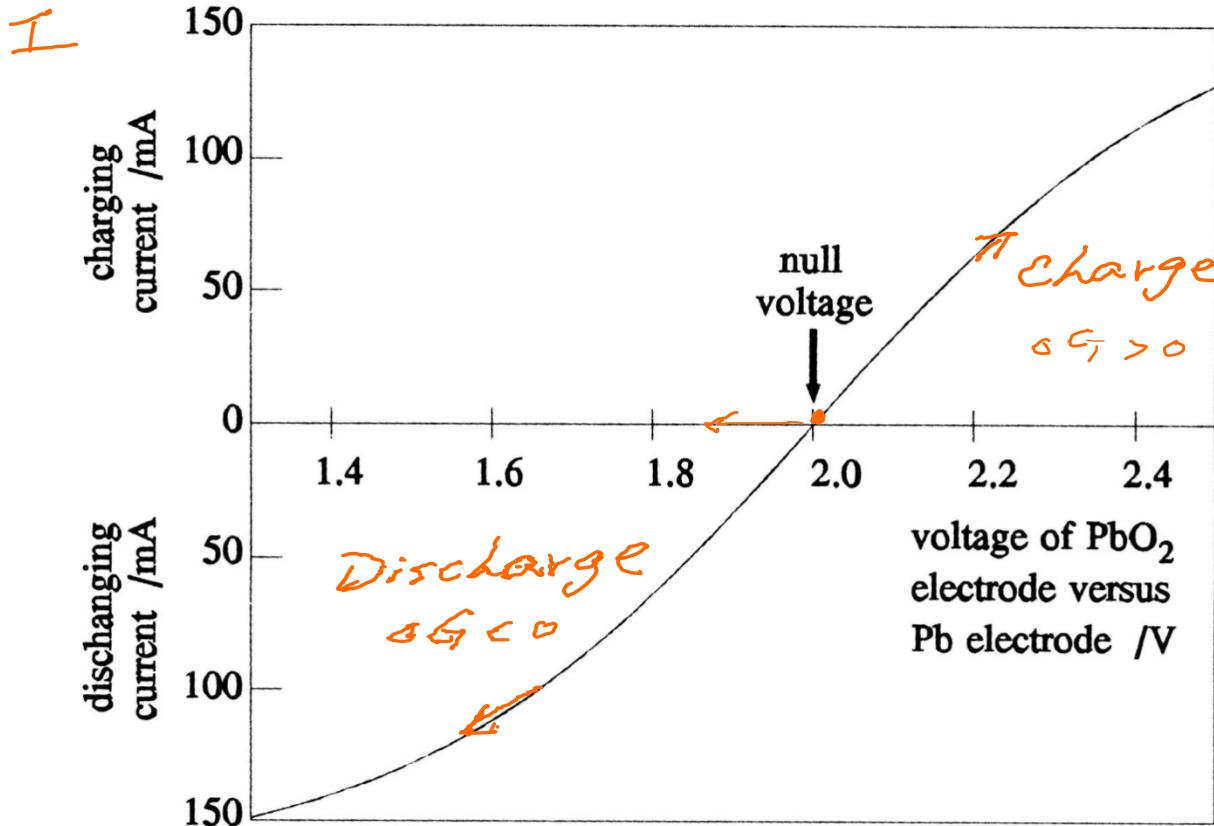
Polarization: a potential departs from its equilibrium potential

Electrolytic cell: $\Delta G > 0$



Voltammogram

(I - V curve) plot



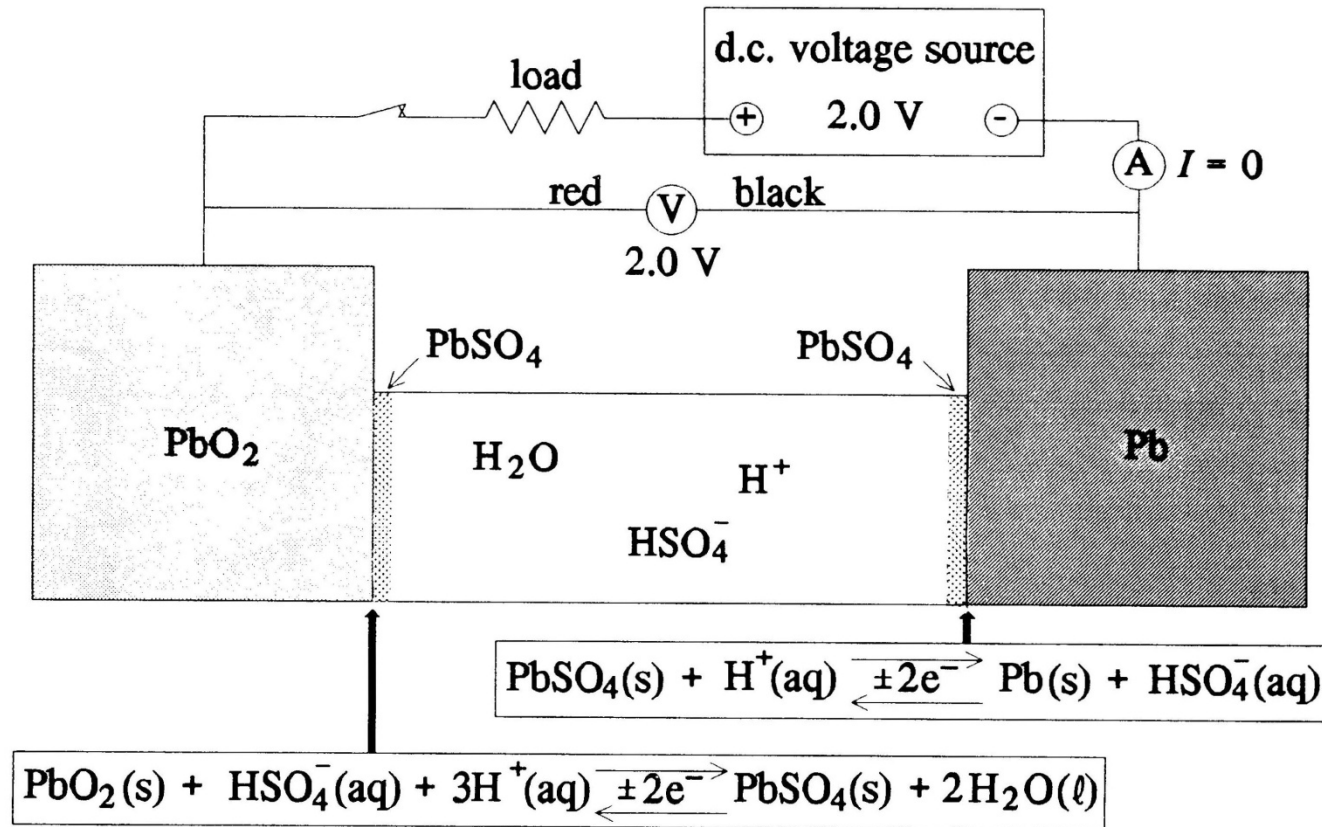
cell voltage:

open circuit potential (OCP) E

(0.0 V) ← E_{cell}

Equilibrium cell voltage; Reversible cell voltage; Rest voltage; Null Voltage; Open-circuit voltage

An Equilibrium Cell



Homogeneous Reactions



$$v_f = k_f C_A$$

$$v_b = k_b C_B$$

$$v_{net} = k_f C_A - k_b C_B$$

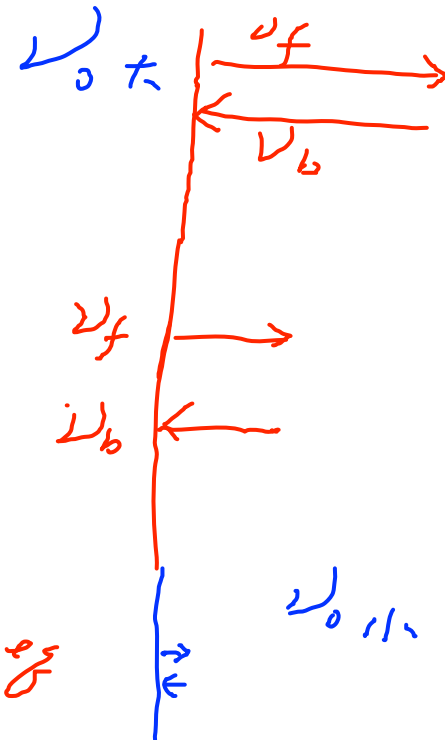
At equilibrium $v_{net} = 0$

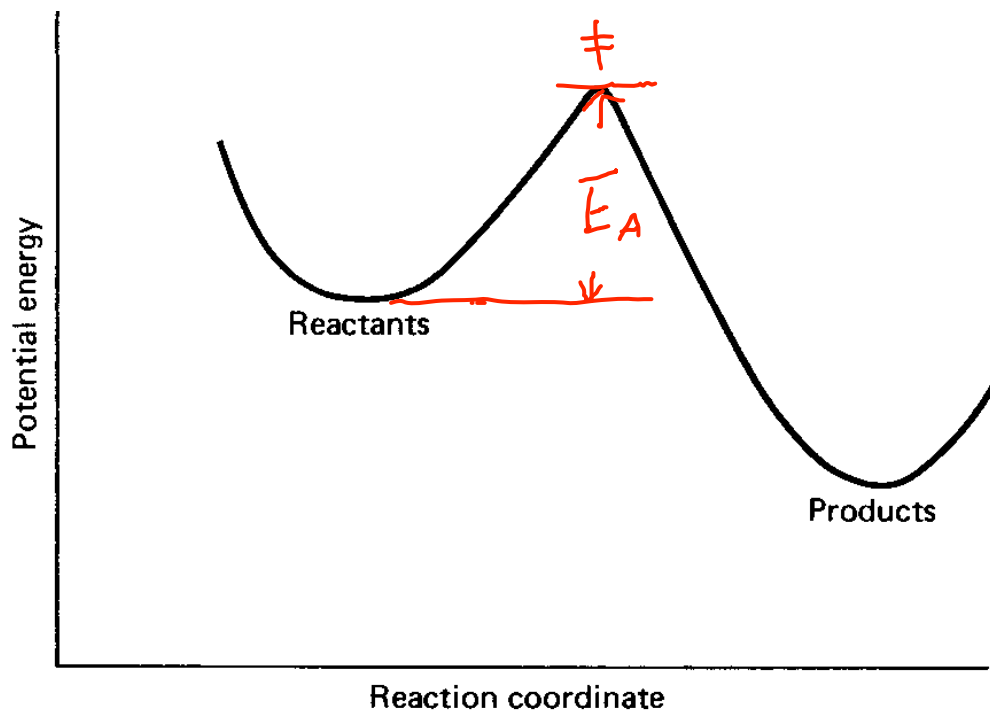
$$K = \frac{k_f}{k_b} = \frac{(C_B)_{eq}}{(C_A)_{eq}}$$

Kinetic
parameter
↑
exchange
velocity

$$v_0 = k_f (C_A)_{eq} = k_b (C_B)_{eq}$$

$$(v_f)_{eq} = (v_b)_{eq}$$





$$k = A e^{-E_A/RT}$$

$$\downarrow$$

$$A' e^{-\Delta G^\ddagger/RT}$$

Transition state
- theory

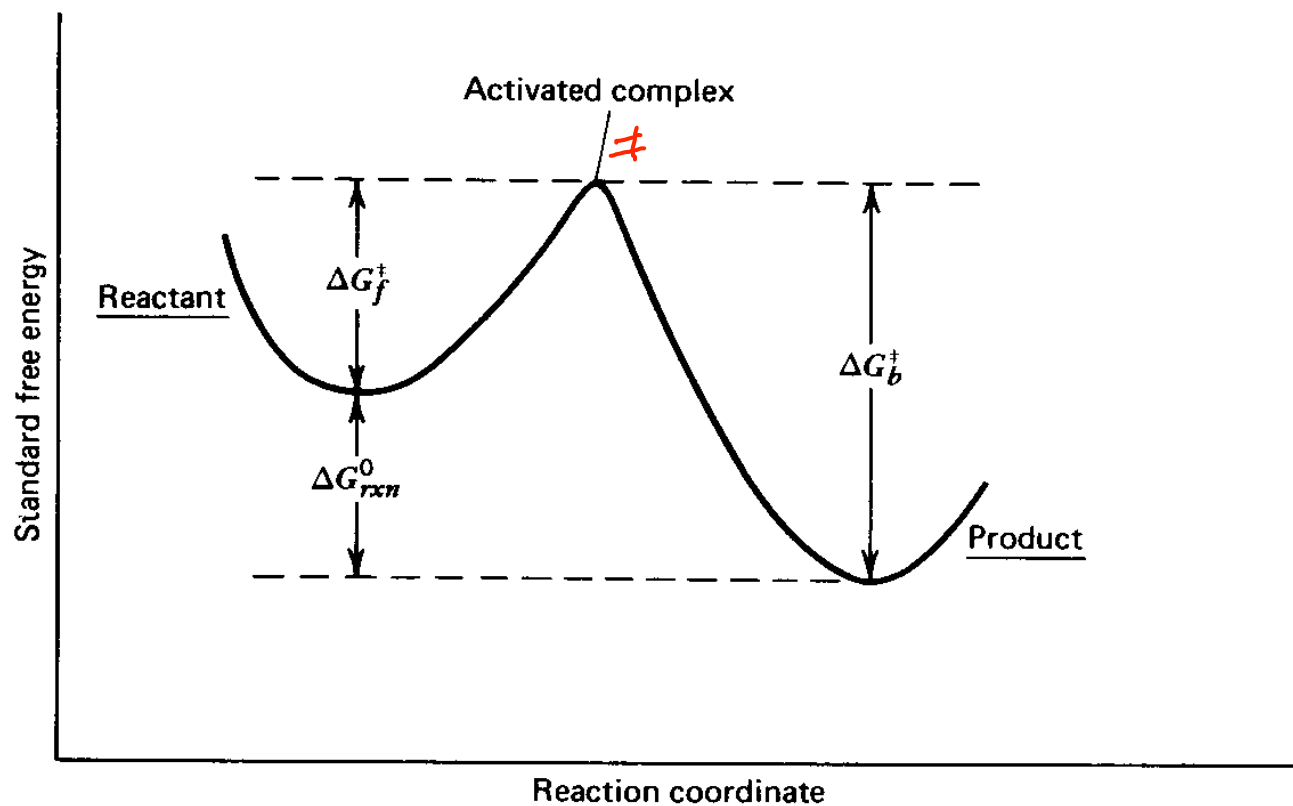
$$k = \kappa \frac{kT}{h} e^{-\Delta G^\ddagger/RT}$$

Chemical rxn

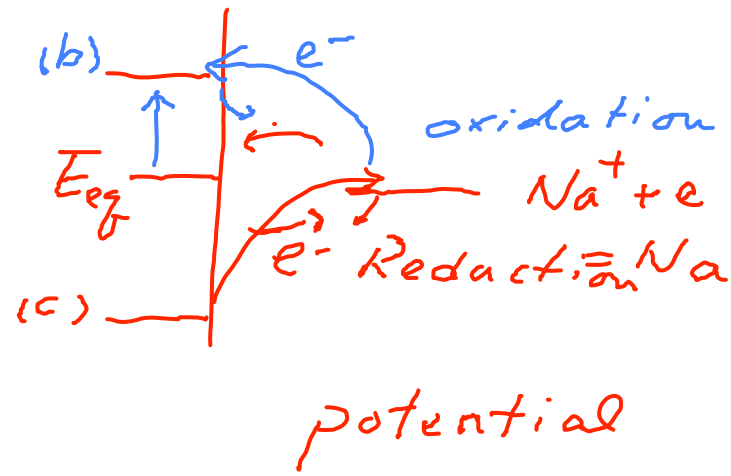
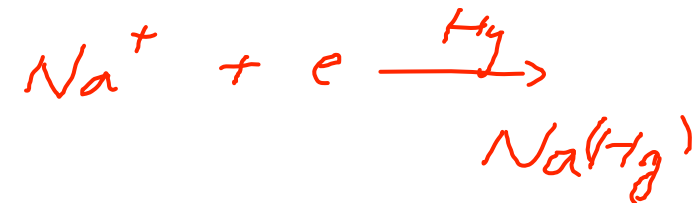
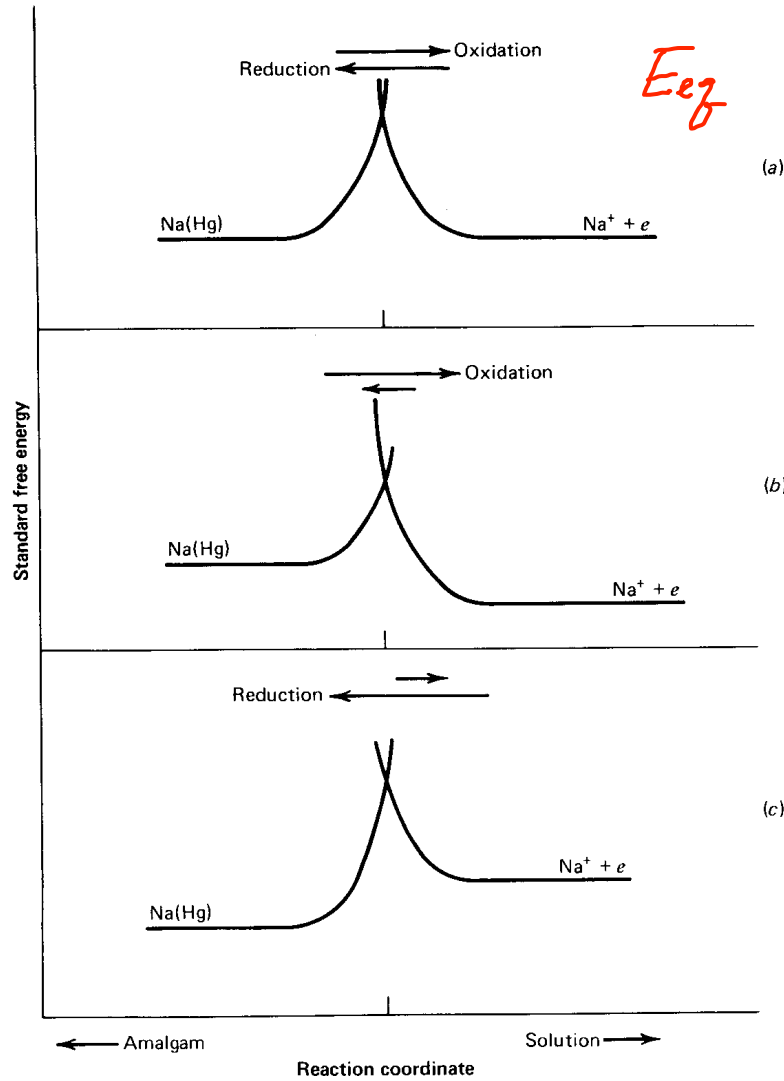
$$\Delta G^\ddagger = f(\text{catalyst})$$

Electrochemical rxn

$$\Delta G^\ddagger = f(\text{cat.}, \text{electrode surface}, E)$$



Effect of potential on energy barriers

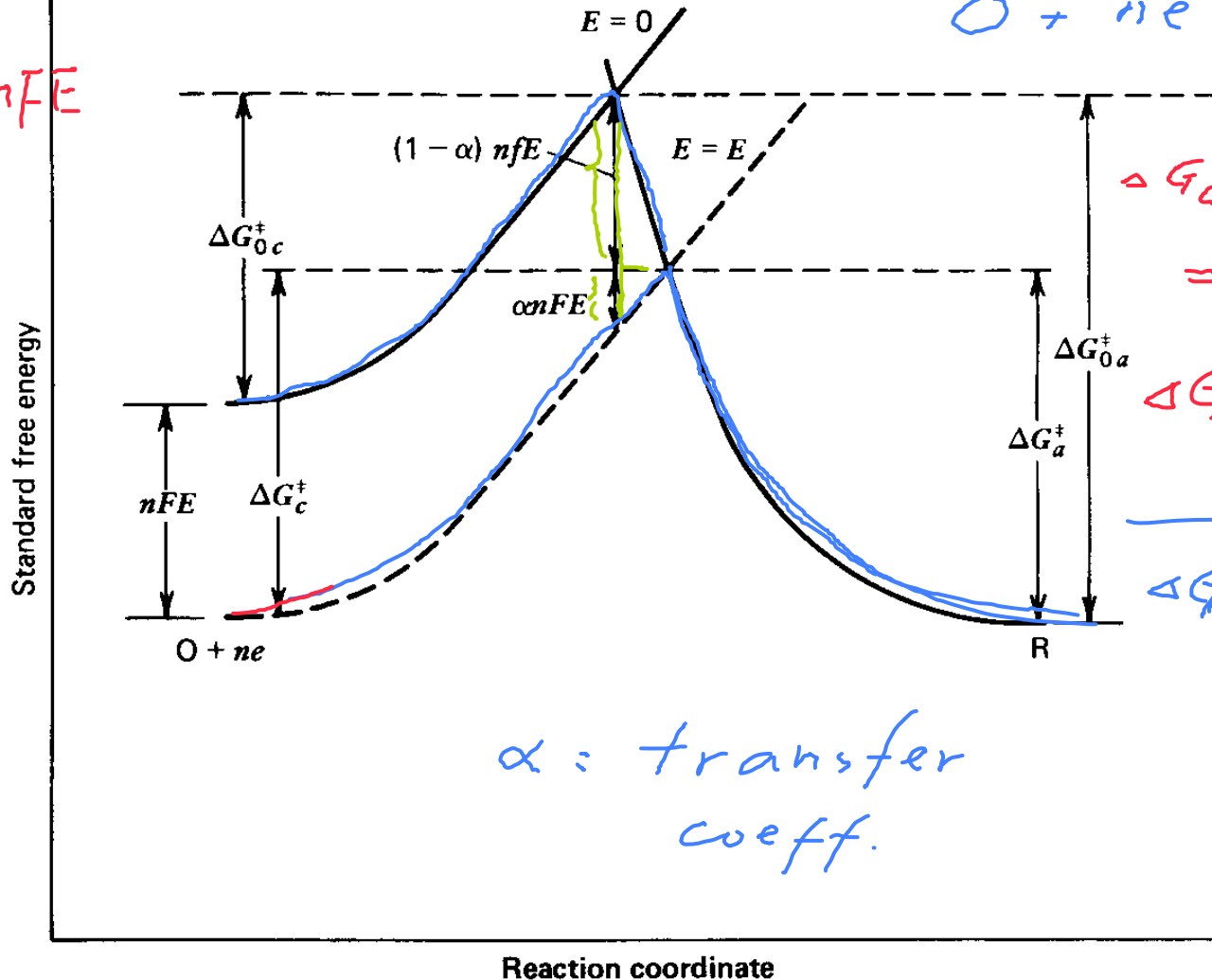


One-step, one-electron reaction

c: cathodic
a: anodic



$$\Delta G = -nFE$$



$$\begin{aligned} \Delta G_c^{\ddagger} &= \Delta G_{0c}^{\ddagger} + (1-\alpha)nFE \\ &= nFE + \Delta G_{0c}^{\ddagger} \end{aligned}$$

$$\Delta G_c^{\ddagger} = \Delta G_{0c}^{\ddagger} + \alpha nFE$$

$$\Delta G_a^{\ddagger} = \Delta G_{0a}^{\ddagger} - (1-\alpha)nFE$$

α : transfer coeff.

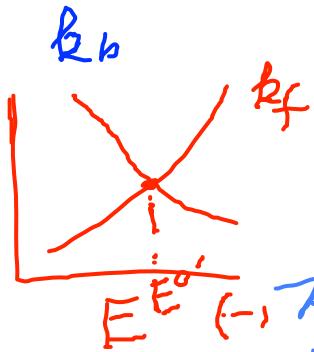


$$k_f = A_f e^{-\Delta G_c^\ddagger / RT}$$

$$k_b = A_b e^{-\Delta G_a^\ddagger / RT}$$

$$f = \frac{F}{RT}$$

$$(n=1)$$



$$k_f = A_f \exp(-\Delta G_c^\ddagger) e^{-\alpha f E}$$

$$k_b = A_b \exp(-\Delta G_a^\ddagger) e^{(1-\alpha) f E}$$

$$C_O(x,t)$$

$$C_R(x,t)$$

$$\frac{i}{nFA} =$$

$$V_{net} = k_f C_O(x,t) - k_b C_R(x,t)$$

$$\frac{\text{mol}}{\text{s} \cdot \text{cm}^2}$$

$$i = nFA (k_f C_O(x,t) - k_b C_R(x,t)) = i_c - i_a$$

$$n=1$$

$$i = FA \left[A_f e^{-\frac{\Delta G_{oc}^\ddagger}{RT}} e^{-\alpha f E} C_O(0,t) - A_b e^{-\frac{\Delta G_{oa}^\ddagger}{RT}} e^{+(1-\alpha) f E} C_R(0,t) \right]$$

at equilibrium, $E = E^{o'}$, $i = 0$

$$k_f C_O^* = k_b C_R^*$$

$$A_f e^{-\frac{\Delta G_{oc}^\ddagger}{RT}} e^{-\alpha f E^{o'}} C_O^*$$

$$k^o = A_b e^{-\frac{\Delta G_{oa}^\ddagger}{RT}} e^{(1-\alpha) f E^{o'}} C_R^*$$

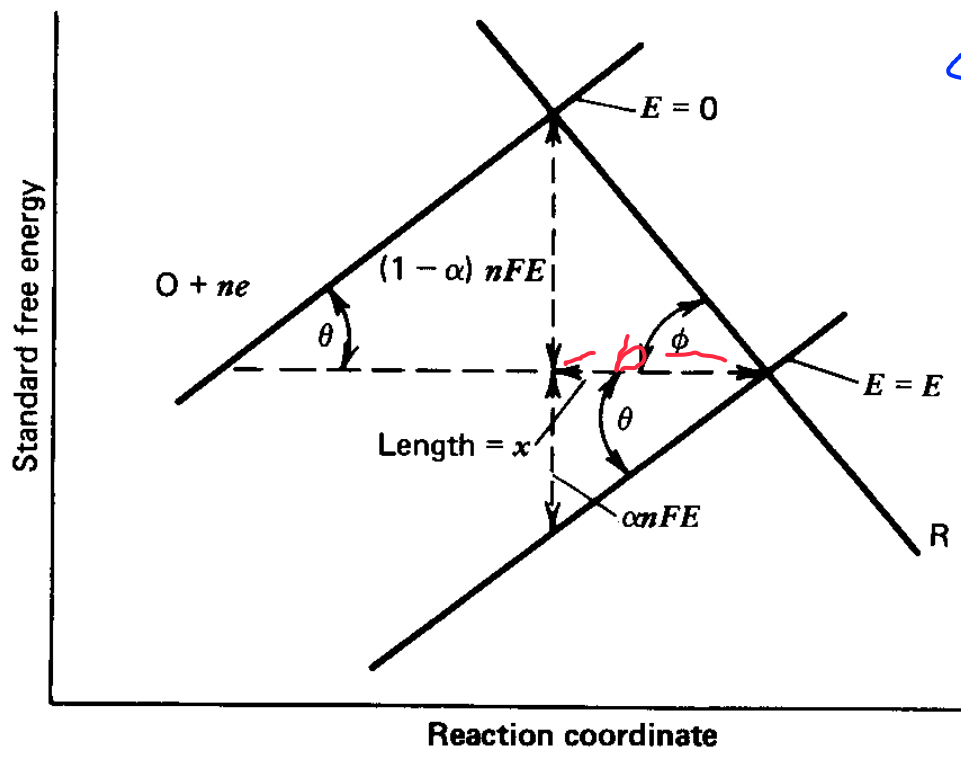
$$i = n F k^o \left[\frac{C_O(0,t)}{C_O^*} e^{-\alpha f (E - E^{o'})} - \frac{C_R(0,t)}{C_R^*} e^{(1-\alpha) f (E - E^{o'})} \right]$$

at $\bar{E} = E^{\circ'}$

$k_f = k_b = k^{\circ}$ standard
rate const

$$i = nFAk^{\circ} \left[C_o(o.t) e^{-\alpha f(E-E^{\circ'})} - C_R(o.t) e^{(1-\alpha) f(E-E^{\circ'})} \right]$$

Effect of angle of intersection of the free energy curves on transfer coefficients

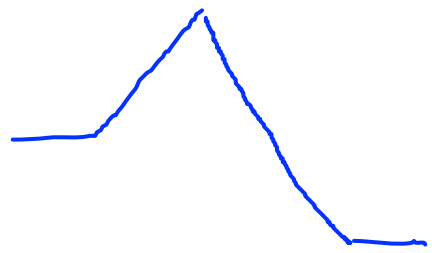


$\alpha =$ transfer coeff.

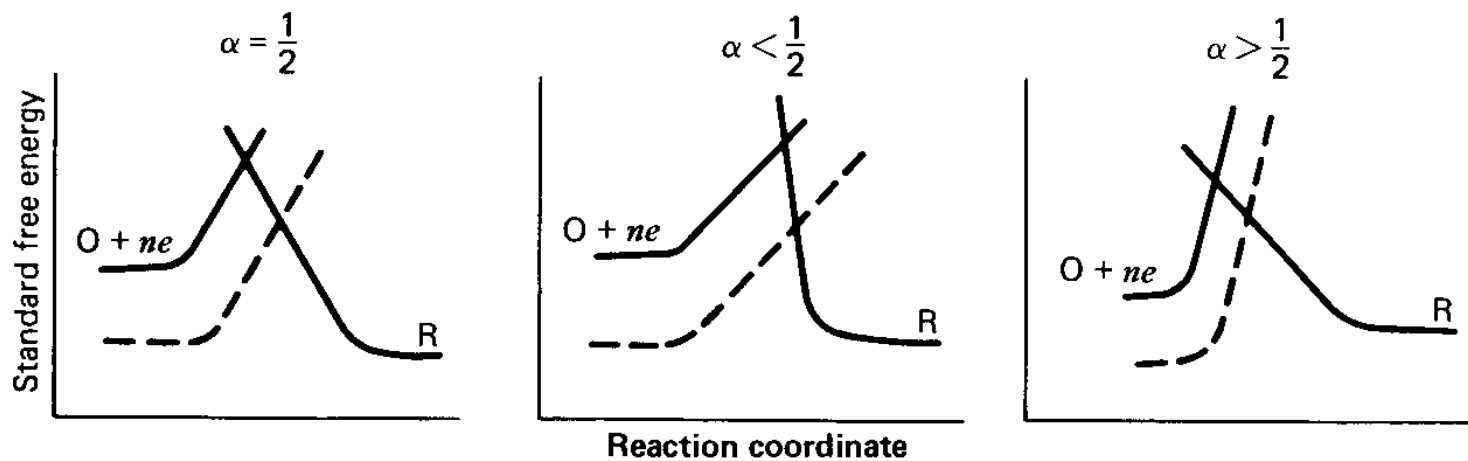
$$\tan \theta = \frac{\alpha FE}{b}$$

$$\tan \phi = \frac{(1 - \alpha) FE}{b}$$

$$\frac{\tan \theta}{\tan \phi} = \frac{\alpha}{1 - \alpha}$$



$$\frac{\tan \theta}{\tan \theta + \tan \phi} = \alpha$$



$$i = FAk^0 \left[C_O(c.t) e^{-\alpha f(E-E^0')} - C_R(c.t) e^{(1-\alpha)f(E-E^0')} \right]$$

$$= i_c - i_a$$

$$0 + e = R$$

at $E = E_{eq}$ ($k_f C_O^* = k_b C_R^*$)
 $i = 0$

Nernst eq

$$i_c(E_{eq}) = i_a(E_{eq}) = i_0$$

exchange current

$$E = E^0' + \frac{RT}{F} \ln \frac{C_O^*}{C_R^*}$$

$$\frac{C_O^*}{C_R^*} = \exp \left[\frac{F}{RT} (E - E^0') \right]$$

$$i = i_0 \left[\frac{C_O(c.t)}{C_O^*} e^{-\alpha f(E-E_{eq})} - \frac{C_R(c.t)}{C_R^*} e^{(1-\alpha)f(E-E_{eq})} \right]$$

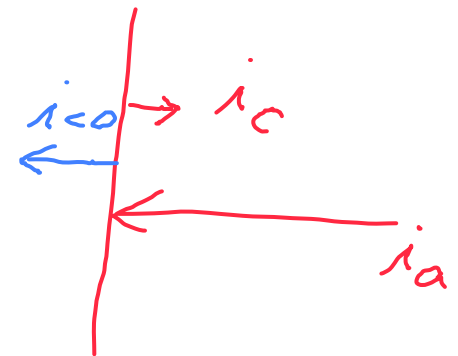
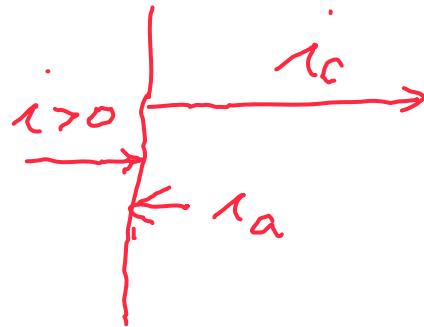
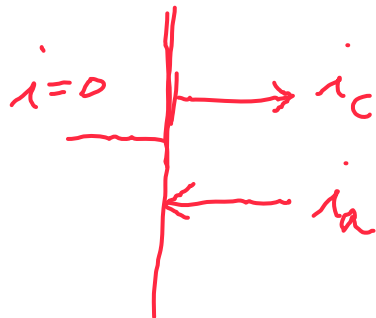
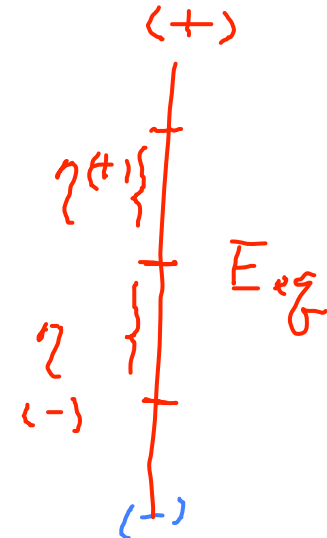
Driving force

$$\eta = \bar{E} - E_{eq}$$

overpotential

i - \bar{E} curve

$$i = i_0 \left[\frac{C_o(0,t)}{C_o^*} e^{-\alpha f \eta} - \frac{C_R(0,t)}{C_R^*} e^{(1-\alpha) f \eta} \right]$$



No Mass transfer effect

$$C_O(0,t) = C_O^*$$

$$C_R(0,t) = C_R^*$$

$$R_m \ll R_{ct}$$

↓
Mass transfer resistance Charge transfer resistance

$$i = i_0 \left[e^{-\alpha f \eta} - e^{(1-\alpha) f \eta} \right]$$

resistance resistance

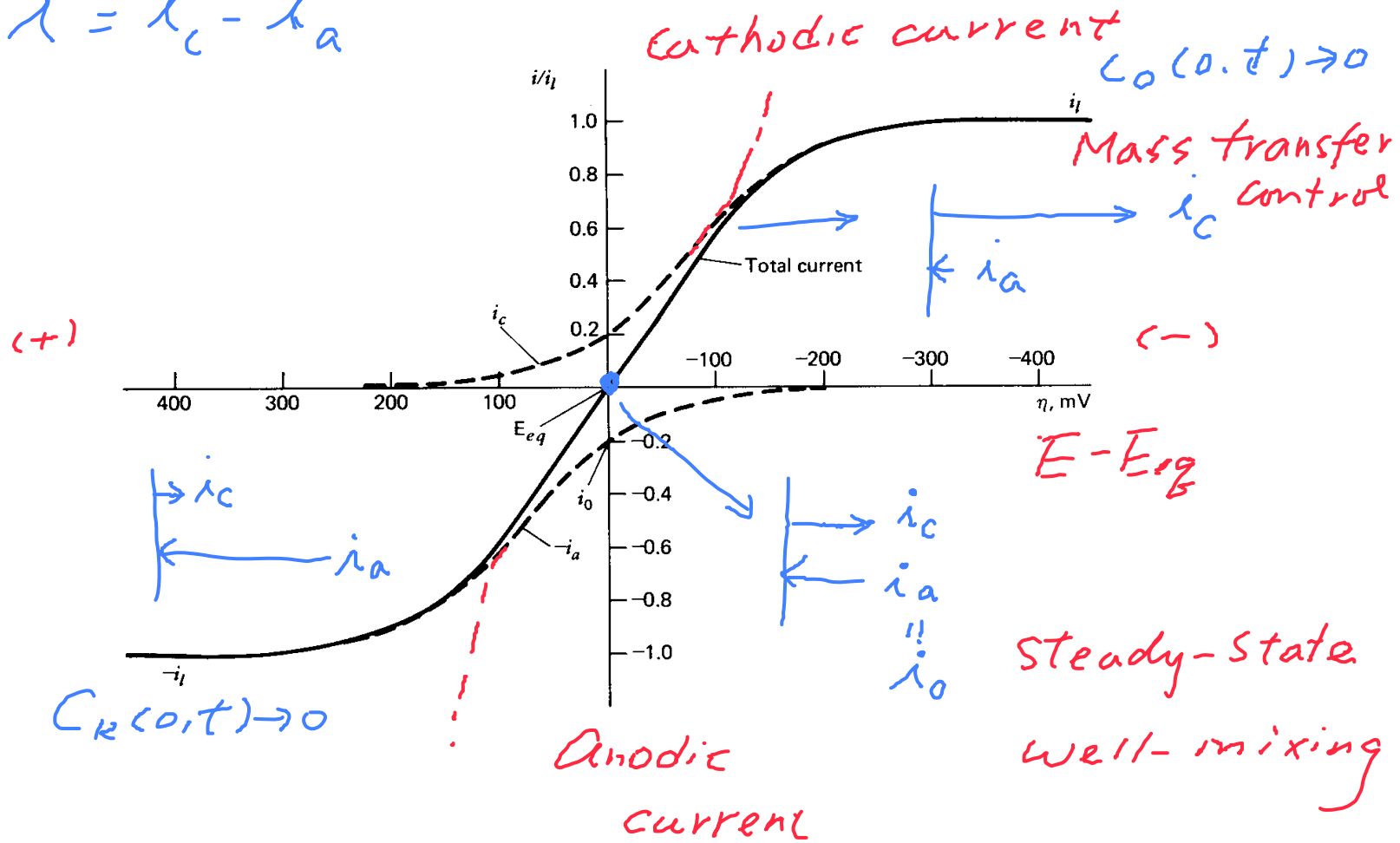
= Butler-Volmer eq

i_0 :

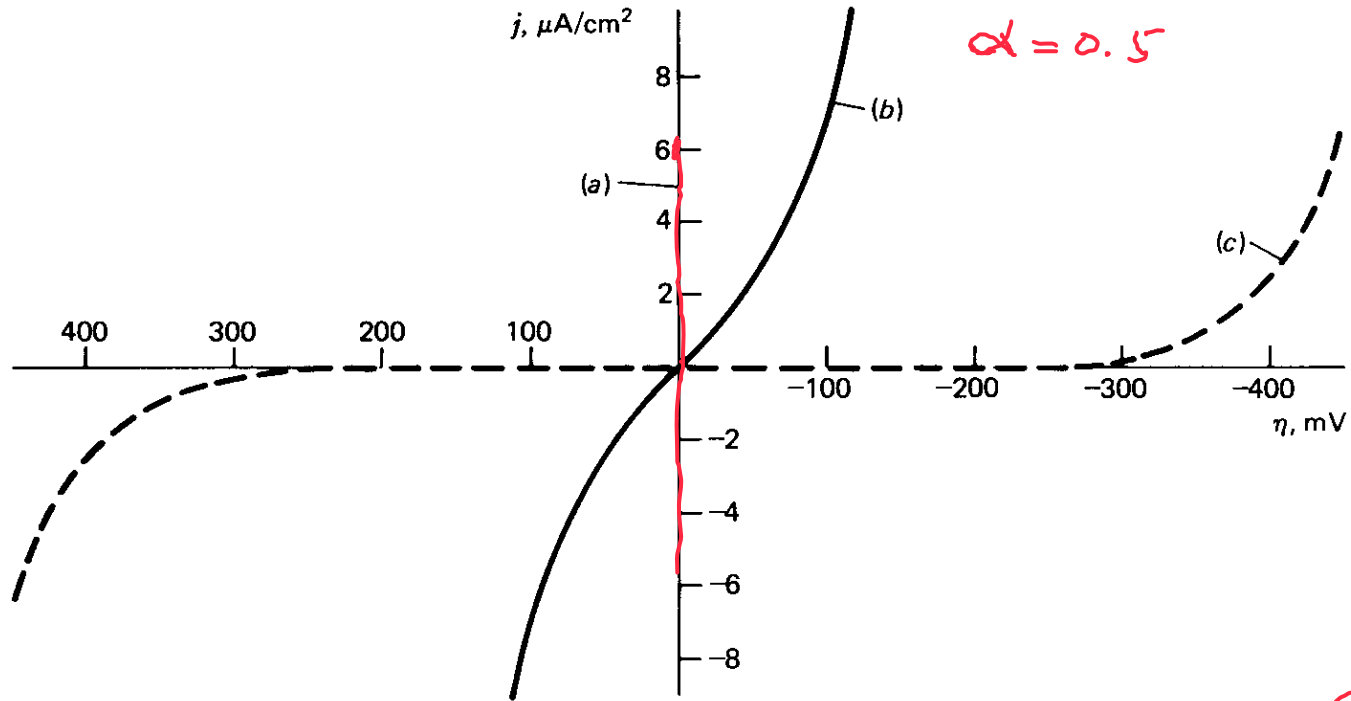
α :

Current-potential curves

$$i = i_c - i_a$$



$j_0: 10^{-3} \sim 10^{-9}$
 (a) (C) A/cm²
 $\alpha = 0.5$

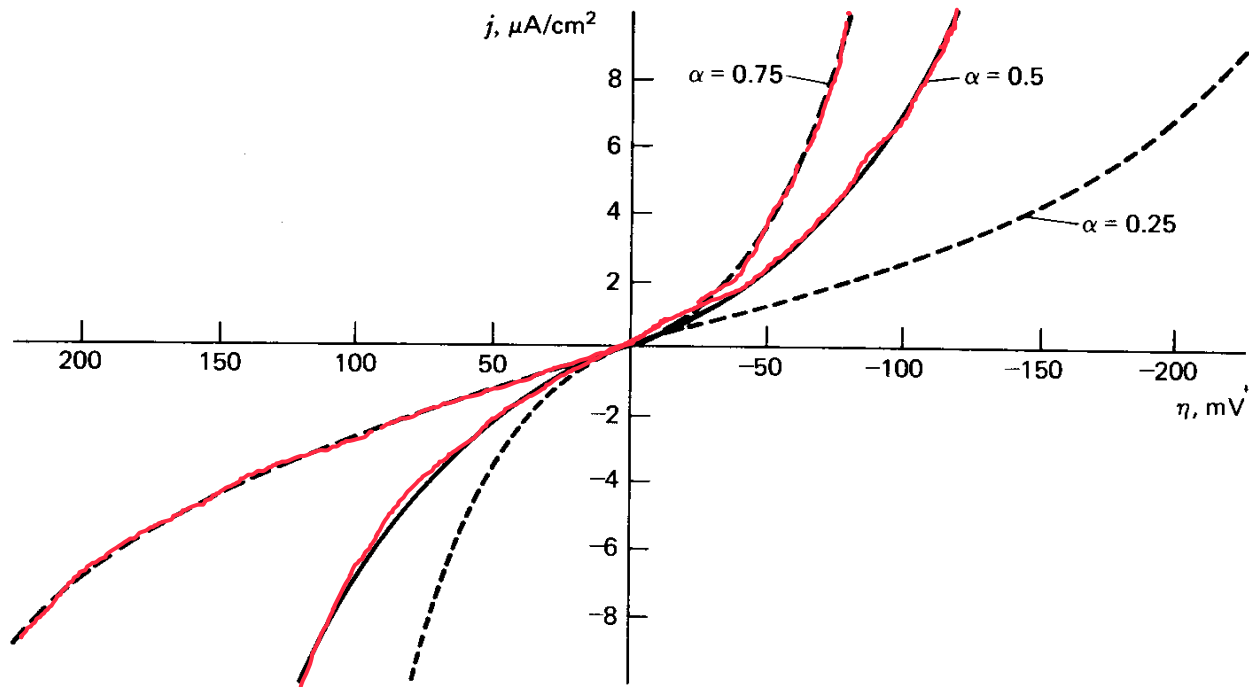


j_0 :
 exchange
 current
 density

$$i = i_0 \left[e^{-\alpha f \eta} - e^{(1-\alpha) f \eta} \right]$$

$$j = j_0 \left[\dots \right]$$

Effect of transfer coefficient



$$i_A = i_0 [e^{-\alpha f \eta} - e^{(1-\alpha) f \eta}]$$

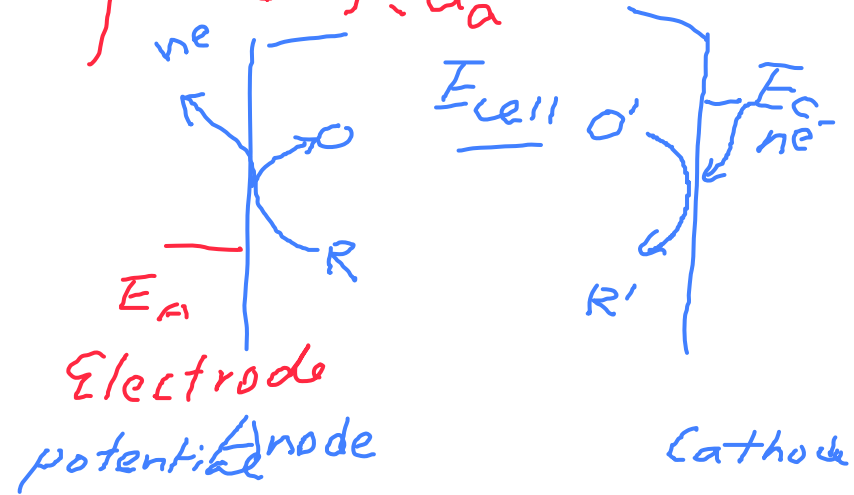
$$i'_C = i_0' [e^{-\alpha' f \eta'} - e^{(1-\alpha') f \eta'}]$$

$$\alpha : \alpha_c$$

$$\alpha : \alpha_a$$

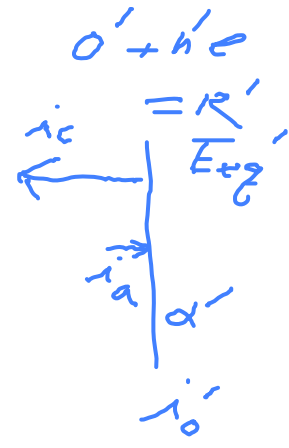
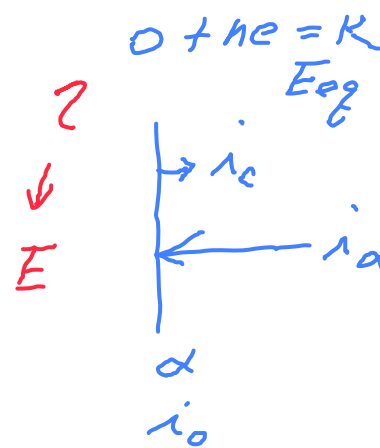
Anode: $\eta = \bar{E}_A - \bar{E}_{eq}$

Cathode: $\eta' = \bar{E}_C - \bar{E}'_{eq}$



$$\bar{E}_{cell} = \bar{E}_C - \bar{E}_A$$

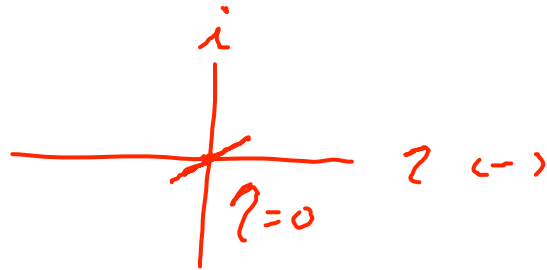
$$i_{measured} = |i_A| = |i'_C|$$



$$i = i_0 \left[e^{-\alpha f \eta} - e^{(1-\alpha) f \eta} \right]$$

Case 1: $\eta \rightarrow 0$ $f = \frac{F}{RT}$

$$i = -i_0 f \eta \Rightarrow R_{ct} = \frac{| \eta |}{i}$$

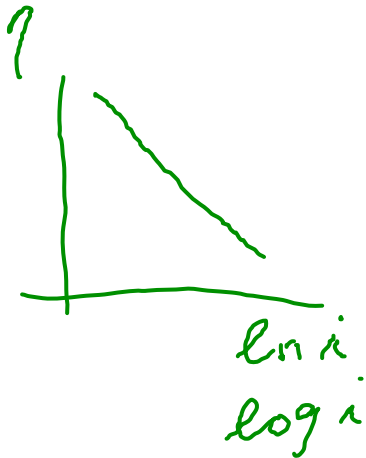


$$= \frac{RT}{F i_0}$$

Case 2: $| \eta | > 118 \text{ mV}$

$$\eta = a + b \log i$$

Tafel



$$\eta (-) : i \doteq i_0 e^{-\alpha f \eta}$$

$$\eta (+) : i \doteq i_0 e^{(1-\alpha) f \eta}$$

$$\ln i = \ln i_0 - \alpha f \eta$$

$$\eta = \frac{RT}{\alpha F} \ln i_0 - \frac{RT}{\alpha F} \ln i = a + b \log i$$

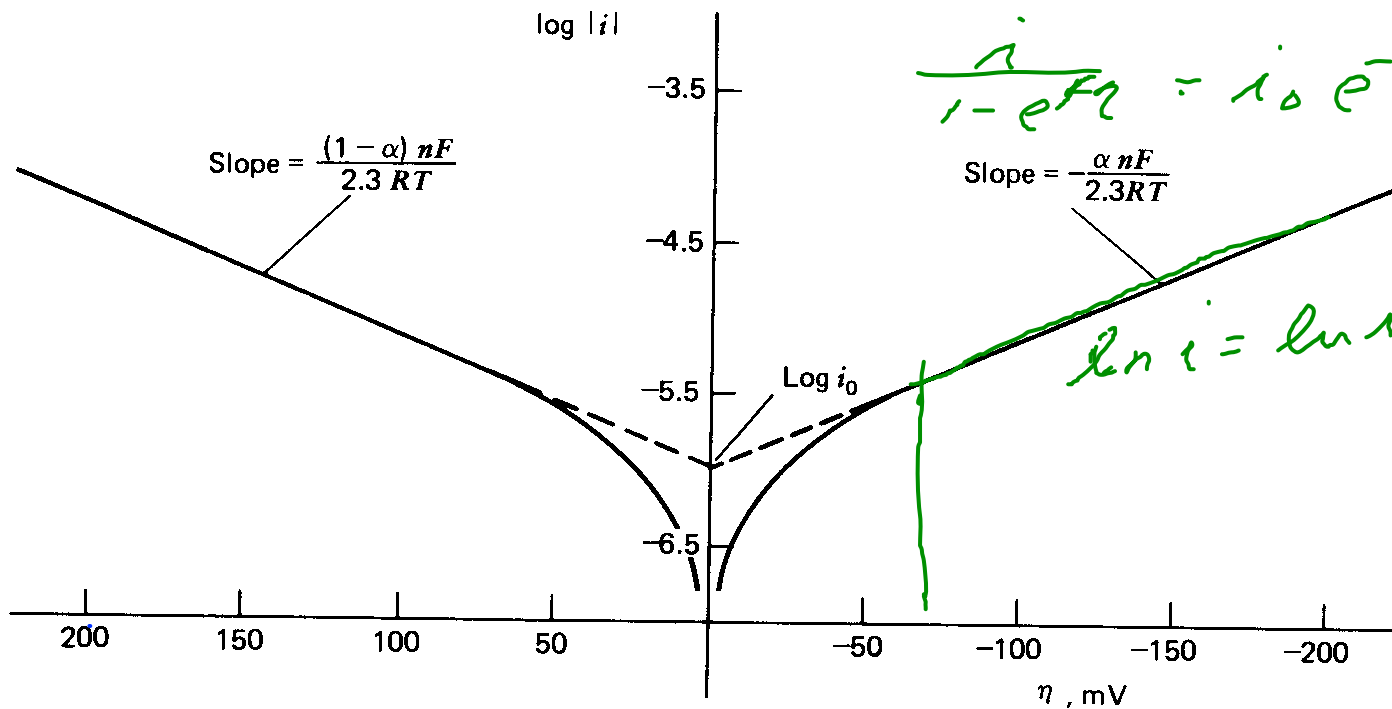
Tafel plots

$$\log \frac{i}{1 - e^{nf\eta}} = \log i_0 - \frac{\alpha n F \eta}{2.3 RT}$$

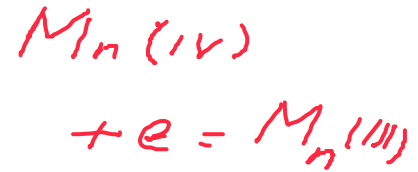
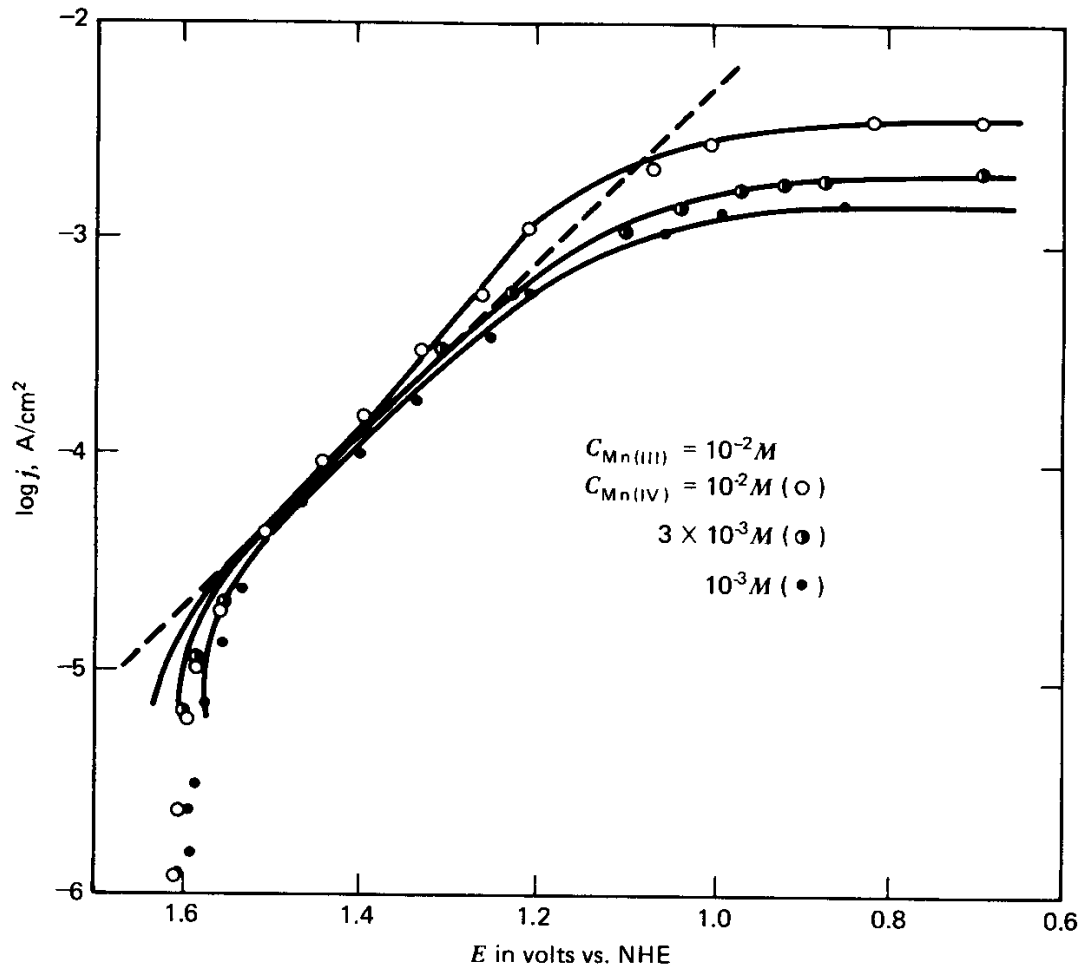
$$i = i_0 [e^{-\alpha f \eta} - e^{(1-\alpha) f \eta}]$$

$$= i_0 e^{-\alpha f \eta} [1 - e^{f \eta}]$$

$$\frac{i}{1 - e^{f \eta}} = i_0 e^{-\alpha f \eta}$$



Tafel plots for the reduction of Mn(IV) to Mn(III)

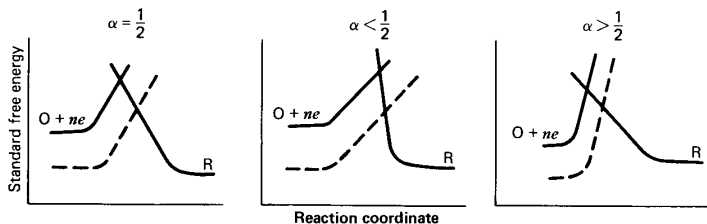
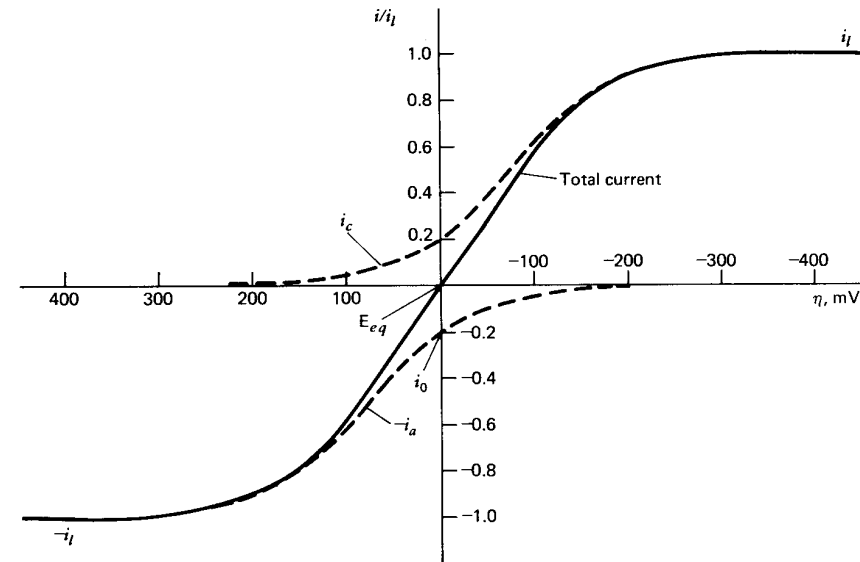


$$I = nFAk_o \{C_o(0,t) \exp[-\alpha nF(E-E_o)/RT] - \{C_R(0,t) \exp[(1-\alpha)nF(E-E_o)/RT]\}$$

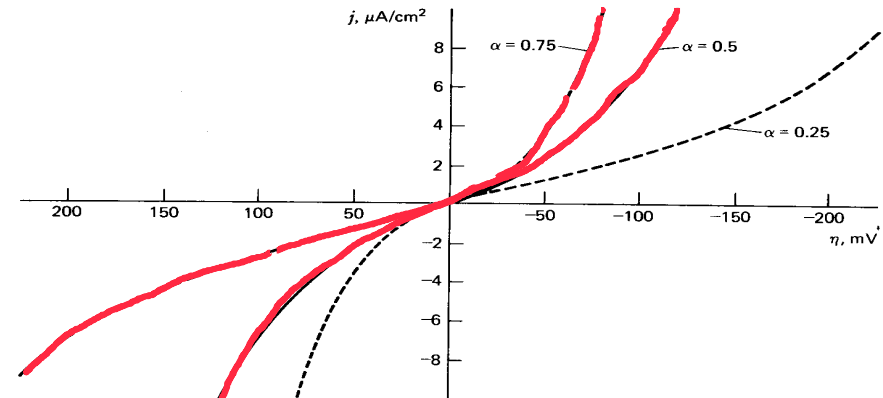
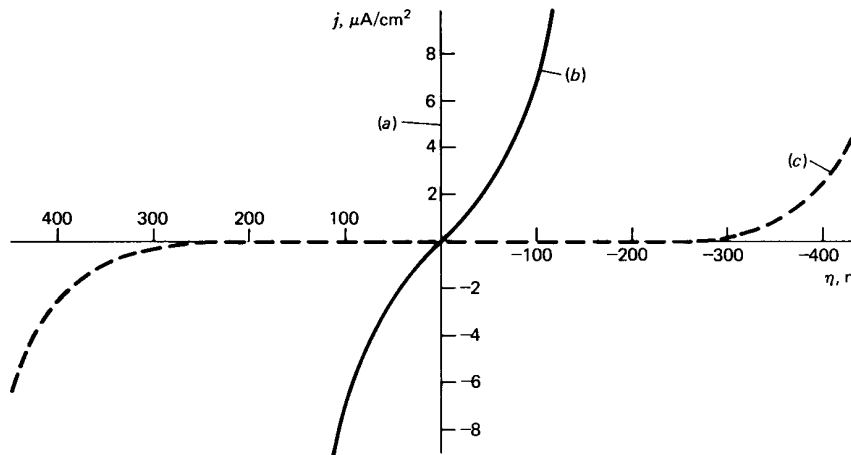
$$= i_o \{C_o(0,t)/C_{o,eq} \exp[-\alpha nF\eta/RT] - \{C_R(0,t)/C_{R,eq} \exp[(1-\alpha)nF\eta /RT]\}$$

$$= i_c - i_a$$

Where i_o = exchange current
 i_c = cathodic current
 i_a = anodic current
 α = transfer coefficient
 $\eta = E - E_{eq}$ = overpotential



$$1. I = I_0 [\exp(-\alpha_c n F \eta / RT) - \exp(\alpha_a n F \eta / RT)]$$



1. At low overpotential region (called "polarization resistance", i.e., when $E \approx E_{eq}$), where the Butler–Volmer equation simplifies to:

$$i = i_0 \frac{nF}{RT} (E - E_{eq})$$

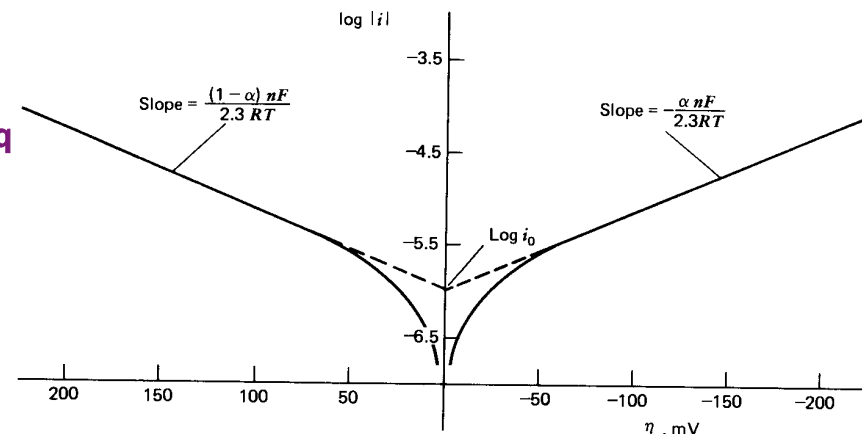
2. At the high overpotential region, where the Butler–Volmer equation simplifies to the **Tafel equation**:

(a) for a cathodic reaction, when $E \ll E_{eq}$,

or
$$E - E_{eq} = a + b \log(i)$$

(b) for an anodic reaction, when $E \gg E_{eq}$

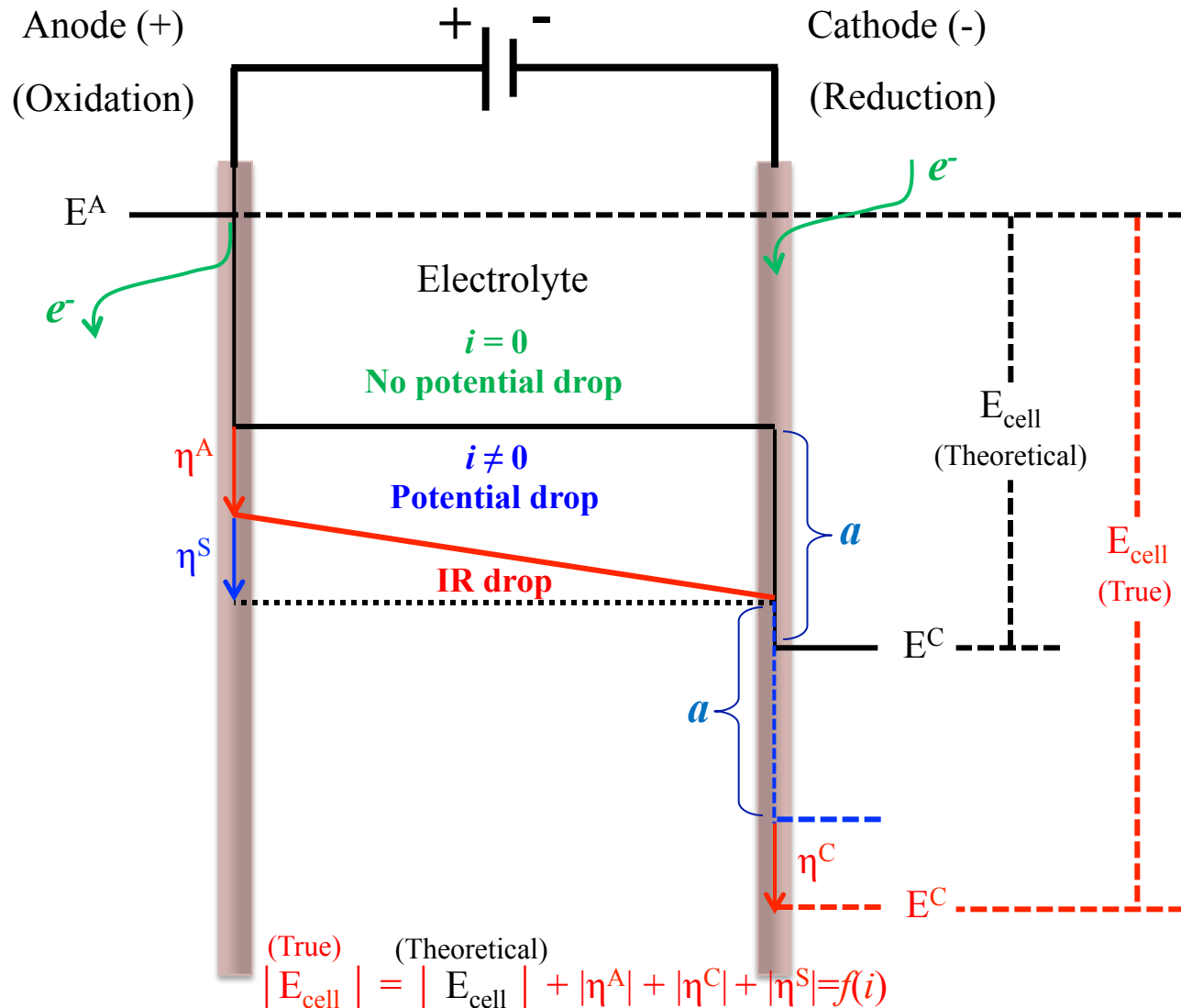
$$E - E_{eq} = a - b \log(i)$$



1. Equilibrium potential (E_{eq})
2. **Open circuit potential (OCP)**
3. Exchange current density (i_o)
4. Transfer coefficient (Symmetric factor) (α)
5. Overpotential s
6. Charge transfer (activation) overpotential or polarization (η_{ct} or η_a)
7. Concentration overpotential or polarization (η_c)
8. Ohmic overpotential or polarization (η_{Ω})

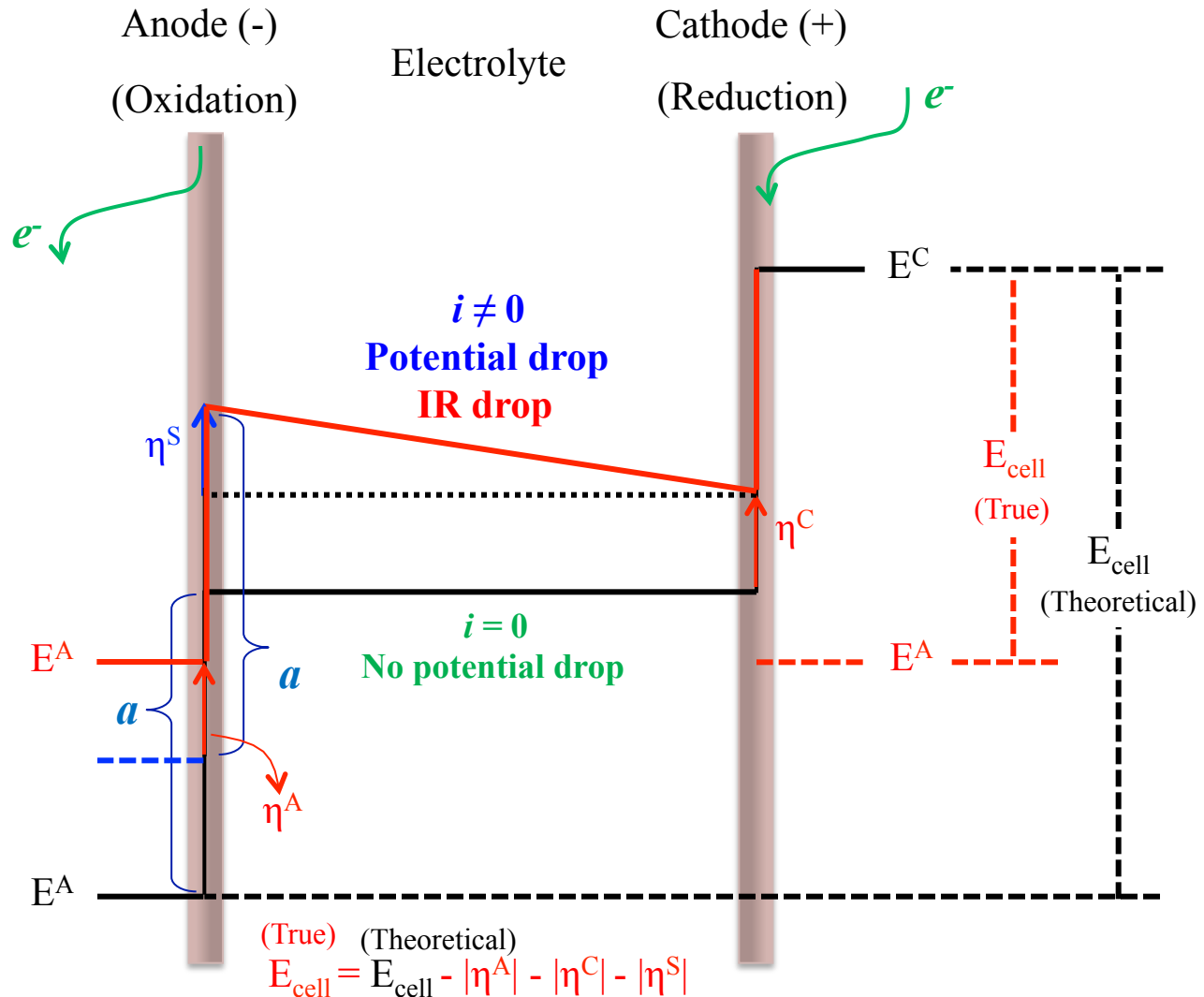
Electrolytic cell ($\Delta G > 0$)

Potential drop (overpotential)



Galvanic cell ($\Delta G < 0$)

Potential drop (overpotential)



Kinetic parameters of electrode reactions

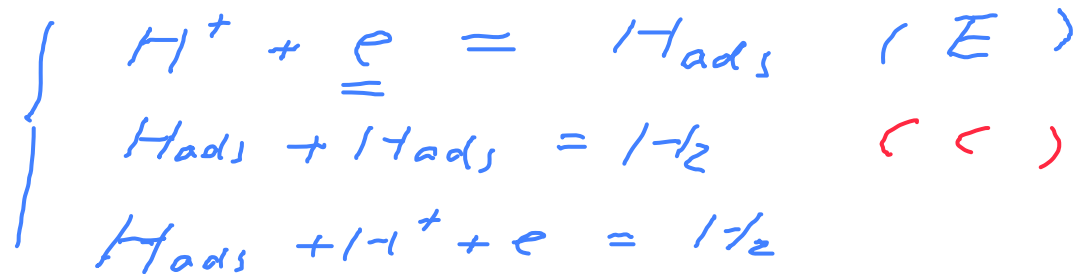
Reaction	Solution	Electrode	α	$k^0/\text{m s}^{-1}$
$\text{Fe}^{3+}(\text{aq}) \xrightleftharpoons{\pm e^-} \text{Fe}^{2+}(\text{aq})$	0.5 M HClO_4	Pt	0.50	9×10^{-8} at 25°C
$\text{Fe}^{3+}(\text{aq}) \xrightleftharpoons{\pm e^-} \text{Fe}^{2+}(\text{aq})$	1.0 M HCl	C	0.59	1.2×10^{-6} at 21°C
$\text{Ce}^{4+}(\text{aq}) \xrightleftharpoons{\pm e^-} \text{Ce}^{3+}(\text{aq})$	1.0 M H_2SO_4	C	0.28	3.8×10^{-6} at 25°C
$\text{V}^{\text{III}}(\text{aq}) \xrightleftharpoons{\pm e^-} \text{V}^{\text{II}}(\text{aq})$	1.0 M HClO_4	Hg	0.52	3.2×10^{-5} at 20°C
$\text{MnO}_4^- (\text{aq}) \xrightleftharpoons{\pm e^-} \text{MnO}_4^{2-} (\text{aq})$	1.0 M KOH	Pt	—	1.2×10^{-6} at 20°C
$\text{Ag}^+(\text{aq}) \xrightleftharpoons{\pm e^-} \text{Ag}(\text{s})$	1.0 M HClO_4	Ag	—	2×10^{-4} at 25°C
$\text{Fe}(\text{CN})_6^{3-} (\text{aq}) \xrightleftharpoons{\pm e^-} \text{Fe}(\text{CN})_6^{4-} (\text{aq})$	1.0 M KNO_3	Pt	0.49	6.6×10^{-4} at 35°C

$$i = i_0 \left[\frac{C_O}{C_O^*} e^{-\alpha n f \eta} - \frac{C_R}{C_R^*} e^{(1-\alpha) n f \eta} \right]$$

$O + n e = R$ (simple one step)

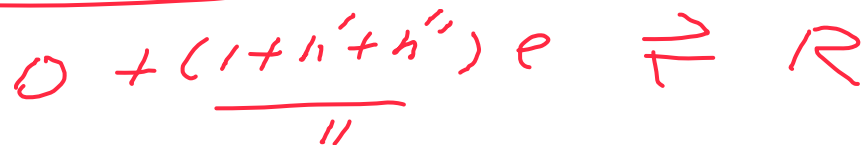


Multi-step rxns



Rate determining electron transfer

Overall rxn



$$i_t \left\{ \begin{array}{l} \leftarrow i_1 = h' i_{rds} \\ \leftarrow i_{rds} \\ \leftarrow i_3 = h'' i_{rds} \end{array} \right.$$

$$i_t = (1 + h' + h'') i_{rds}$$

pseudo steady-state assumption

$$i_{rds} = n F A k_{rds}^0 [C_{O'}(0,t) e^{-\alpha f (E - E_{rds}^0)} - C_{R'} e^{(1-\alpha) f (E - E_{rds}^0)}]$$

Multi-step process at equilibrium

$$r_1 = k_1^{\circ} \dots \Rightarrow \frac{r_1}{k_1^{\circ}} \rightarrow 0$$

$$\parallel$$

$$r_2 = k_{rds}^{\circ} \dots$$

$$\parallel$$

$$r_3 = k_3^{\circ} \dots$$

$$\frac{r_3}{k_3^{\circ}} \rightarrow 0$$

$$k_1^{\circ}, k_3^{\circ} \gg k_{rds}^{\circ}$$



$$R' + n''e = R$$

$$E_{eq} = E_1^{\circ'} + \frac{RT}{n'F} \ln \frac{C_0}{C_0'}$$

$$C_0' = C_0 e^{-(E_{eq} - E_1^{\circ'}) n'F / RT}$$

$$C_{R'} = C_R e^{(E_{eq} - E_3^{\circ'}) n''F / RT}$$

$$C_{R'} = C_0' e^{-(E_{eq} - E_{rds}^{\circ'}) F / RT}$$

Nernstian Multistep processes

$$i = nFAk_{rds} \left[\frac{C_O}{C_O} e^{-\frac{(E - E_1^{o'})nF}{RT} - \frac{\alpha F(E - E_{rds}^{o'})}{RT}} - \frac{C_R}{C_O} e^{-\frac{(n' + \alpha)FE}{RT} + \frac{(n'E_1^{o'} + \alpha E_{rds}^{o'})F}{RT}} \right]$$

$$- \frac{C_R}{C_O} e^{-\frac{(E - E_3^{o'})n''F}{RT} + \frac{(1 - \alpha)F(E - E_{rds}^{o'})}{RT}}$$

Formal potential $E = E^{o'}$

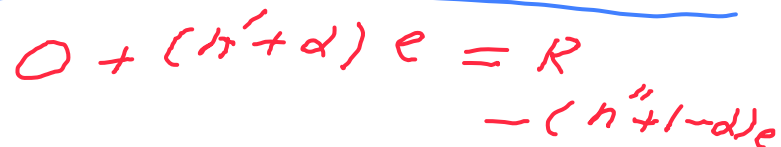
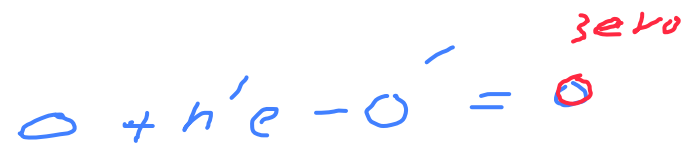
$$\frac{C_R}{C_O} e^{-\frac{(n'' + (1 - \alpha))FE}{RT} - \frac{(n''E_3^{o'} + (1 - \alpha)E_{rds}^{o'})F}{RT}}$$

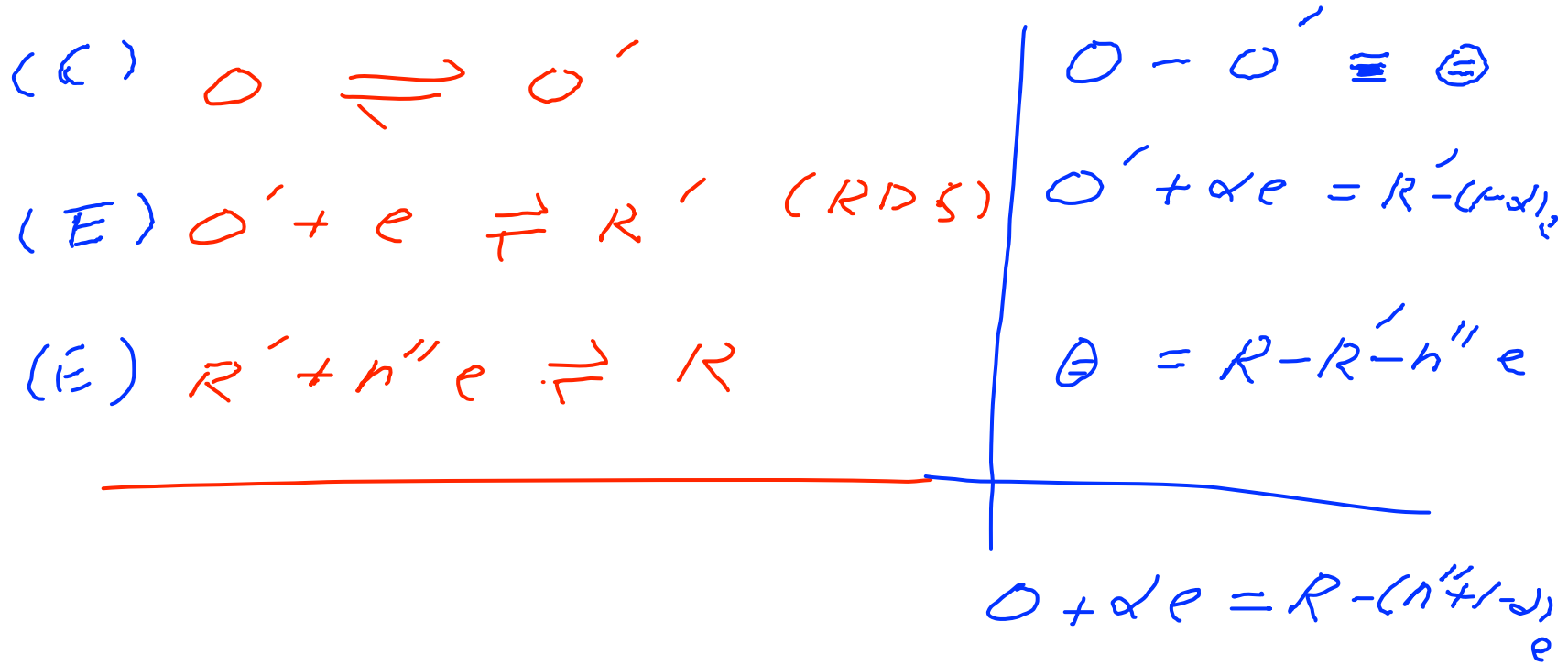
$$C_O = C_R = 1$$

$$E^{o'} = \frac{E_{rds}^{o'} + n'E_1^{o'} + n''E_3^{o'}}{n} \quad 0 + ne = R$$

$$i = nFA [k_f C_O - k_b C_R]$$

$$i = i_0 \left[\frac{C_0}{C_0^*} e^{-(n'+\alpha)f\eta} - \frac{C_R}{C_R^*} e^{(n''+1-\alpha)f\eta} \right]$$



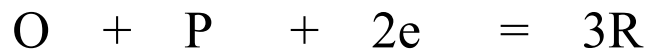


$$i = i_0 \left[\frac{C_O}{C_{O'}^*} e^{-\alpha f \eta} - \frac{C_R}{C_R^*} e^{(n''+1-\alpha) f \eta} \right]$$

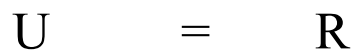
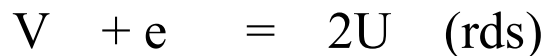
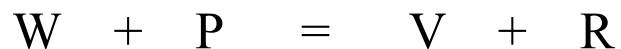
Key steps to derive the kinetic equations for a complex reaction

- (1) Write down the rate determining step.
- (2) Each of the mechanistic steps that precedes the rds is in equilibrium.
- (3) Conversely, rewrite all the steps that follow the rds by transferring, with a sign change, all the species from the left-hand side to the right hand side.
- (4) Leaving the rds unmodified, multiply each of the other equations, if necessary, by a small integer such that the intermediates will disappear when rule (V) below is implemented.
- (5) Add the equations to generate the stoichiometric equation.

Overall reaction



ECEC mechanism



$$\mathbf{O} - \mathbf{W} + \mathbf{e} =$$

$$\mathbf{W} + \mathbf{P} - \mathbf{V} - \mathbf{R} =$$

$$\mathbf{V} + \alpha \mathbf{e} = 2\mathbf{U} - (1 - \alpha)\mathbf{e} \quad (\text{rds})$$

$$= 2\mathbf{R} - 2\mathbf{U}$$

They sum to

$$\mathbf{O} + \mathbf{P} - \mathbf{R} + (1 + \alpha)\mathbf{e} = 2\mathbf{R} - (1 - \alpha)\mathbf{e}$$

$\mathbf{i} =$

$$2Fk[(C^s_R)^2/C^0 \exp\{(1 - \alpha)nF(E - E^0)/RT\} - C^s_O C^s_P / C^s_R \exp\{-(1 + \alpha)nF(E - E^0)/RT\}]$$